

POROUS SQUEEZE FILM BEARING WITH ROUGH SURFACES LUBRICATED BY A BINGHAM FLUID

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In the paper the effect of both bearing surfaces and the porosity of one bearing surface on the pressure distribution and load-carrying capacity of a squeeze film bearing is discussed. The equations of motion of a Bingham fluid in a bearing clearance and in a porous layer are presented. Using the Morgan-Cameron approximation and Christensen theory of rough lubrication the modified Reynolds equation is obtained. The analytical solutions of this equation for a squeeze film bearing are presented. As a result one obtains the formulae expressing pressure distribution and load-carrying capacity. A thrust radial bearing is considered as a numerical example.

Key words: viscoplastic fluid, Bingham model, thrust bearing, porous layer, Christensen roughness.

1. Introduction

Steady state radial flows and time-dependent squeezing flows of viscoplastic fluids are encountered in a variety of fields (Covey and Stanmore, 1981; Dai and Bird, 1981; Lipscomb and Denn, 1984). These flows are found in fabrication operations such as stamping, injection molding, and sheet forming. Also, material properties of highly viscous fluids are measured with a device called the “plastometer” which incorporates a parallel-disk squeeze flow geometry (Covey and Stanmore, 1981). In addition, such flows are encountered in lubrication systems, and there is a considerable interest as to the degree in which viscoplastic additives enhance the load-bearing capacity of a lubricant.

The flows of Newtonian fluids in the clearance of a thrust bearing with impermeable surfaces have been examined theoretically. The bearing walls have been modelled as two disks, two conical or spherical surfaces. The more general case is established by the bearing formed by two surfaces of revolution (Walicka, 1994).

Porous bearings have been widely used in industry for a long time (Bujurke *et al.*, 1987; Etsion, 1994; Morgan and Cameron, 1957; Prakash and Vij, 1973; Shukla and Isa, 1978). Basing on the Darcy model Morgan and Cameron (1957) first presented theoretical research on these bearings.

Lately the problem of curvilinear bearings with porous walls lubricated by a Bingham fluid was taken up by Walicka (2011).

In recent years, a considerable amount of tribology research has been devoted to the study of the effect of surface roughness or geometric imperfections on hydrodynamic lubrication because the bearings surfaces, in practice, are all rough and the height of the roughness asperities may have the same order as the mean bearing clearance. Under these conditions, the surface roughness affects the bearing performance considerably.

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The work in this area has mainly been confined to impermeable surfaces. The well-established stochastic theory of hydrodynamic lubrication of rough surfaces developed by Christensen (1970) formed the basis of this paper. In a series of works (Bujurke *et al.*, 2007; Lin, 2000; 2001; Prakash and Tiwari, 1985; Walicka 2009; 2012; Walicka and Walicki, 2002a; 2002b) the Christensen model was applied to the study of the surface roughness of various geometrical configurations.

To get a better insight into the effect of surface roughness in porous bearings, Prakash and Tiwari (1984) developed a stochastic theory of hydrodynamic lubrication of rough surfaces proposed by Christensen (1970). The modified Reynolds equation (Gurujan and Prakash, 1999) applicable to two types of directional roughness structure were used by Walicka and Walicki (2002a; 2002b) to find bearing parameters for the squeeze film between two curvilinear surfaces.

In this paper a Bingham fluid is used to describe the flow of a lubricant. The modified Reynolds equation is derived and its solution for the curvilinear thrust bearing is presented. The analysis is based on the assumption that the porous matrix consists of a system of capillaries of very small radii which allows a generalization of the Darcy law and the use of the Morgan-Cameron approximation for the flow in a porous layer. According to the Christensen stochastic model (1970), different forms of Reynolds equations are derived to take account of various types of surface roughness. Analytical solutions for the film pressure are presented for the longitudinal and circumferential roughness patterns.

2. Derivation of the modified Reynolds equation for a viscoplastic lubricant

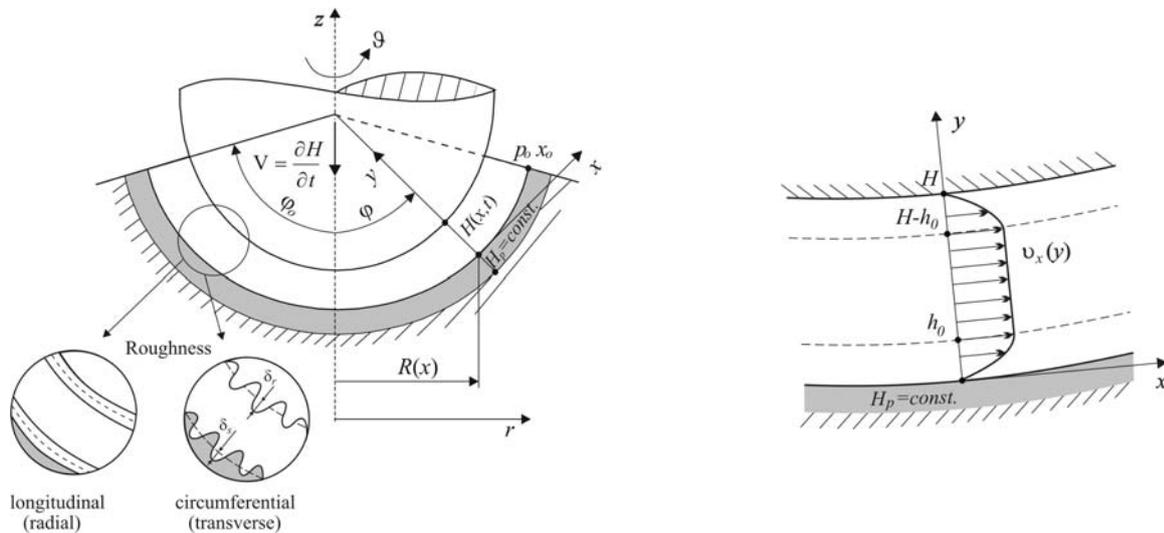


Fig. 1. Configuration of a curvilinear thrust bearing with one porous wall.

Let us consider a thrust bearing with a curvilinear profile of the working surfaces shown in Fig. 4. The upper bound of a porous layer is described by the function $R(x)$ which denotes the radius of this bound. The nominal bearing clearance thickness is given by the function $h(x, t)$, while the porous layer thickness is given by $H_p = \text{const.}$

The expression for the film thickness is considered to be made up of two parts

$$H = h(x, t) + h_s(x, \vartheta, \xi) \quad (2.1)$$

where $h(x, t)$ represents the nominal smooth part of the film geometry, while $h_s = \delta_r + \delta_s$ denotes the random part resulting from the surface roughness asperities measured from the nominal level, ξ describes a

random variable which characterizes the definite roughness arrangement. An intrinsic curvilinear orthogonal coordinate system x, ϑ, y linked with the upper surface of a porous layer is also presented in Fig.1.

Taking into account the considerations of the works (Walicka, 2002; 2011; Walicki, 2005) one may present the equation of continuity and the equations of motion of a Bingham fluid for axial symmetry in the form

$$\frac{1}{R} \frac{\partial (Rv_x)}{\partial x} + \frac{\partial v_y}{\partial y} = 0, \tag{2.2}$$

$$\frac{\partial \Lambda_{xy}}{\partial y} = \frac{\partial p}{\partial x}, \quad \frac{\partial p}{\partial y} = 0. \tag{2.3}$$

The non-zero component of the stress tensor is

$$\Lambda_{yx} = S \left[\tau_0 + \left| \mu \frac{\partial v_x}{\partial y} \right| \right] \tag{2.4}$$

and $S = \text{sgn} \left(\frac{\partial v_x}{\partial y} \right)$; the signum function (sgn) takes the value $+1$ for a positive argument $\left(\frac{\partial v_x}{\partial y} > 0 \text{ for } y \leq h_0 \right)$ and -1 for a negative argument $\left(\frac{\partial v_x}{\partial y} < 0 \text{ for } y \leq H - h_0 \right)$.

In the flow of fluid with yield shear stress there exists a quasi-solid core bounded by surfaces lying at

$$y = h_0 \quad \text{or} \quad y = H - h_0 \quad \text{for which the shear stress is: } \left| \Lambda_{yx} \right| = \tau_0.$$

The problem statement is complete after specification of boundary conditions which are

$$\begin{aligned} v_x(x, 0, t) &= 0, & v_x(x, H, t) &= 0, \\ v_y(x, 0, t) &= V, & v_y(x, H, t) &= \frac{\partial H}{\partial t} = \dot{H}, \\ \frac{\partial p}{\partial x} \Big|_{x=0} &= 0 & p(x_o) &= p_o; \end{aligned} \tag{2.5}$$

here V is the lubricant velocity on the upper boundary of the porous matrix.

Solving Eqs (2.2)-(2.4) one obtains the following Reynolds equation [detailed solution may be found in (Walicka, 2011)]

$$\frac{1}{R} \frac{\partial}{\partial x} \left[Rh^3 \left(-\frac{\partial p}{\partial x} \right) \Phi(\chi) \right] = -12\mu(\dot{H} - V) \tag{2.6}$$

where

$$\chi = \frac{\tau_0}{\tau_w}, \quad \tau_w = \frac{H}{2} \left(-\frac{\partial p}{\partial x} \right), \quad \tau_0 = \left(\frac{H}{2} - h_0 \right) \left(-\frac{\partial p}{\partial x} \right), \quad \chi = \frac{2\tau_0}{\left(-H \frac{\partial p}{\partial x} \right)}; \quad (2.7)$$

τ_w - is the shear stress on the clearance wall and

$$\Phi(\chi) = 1 - \frac{3}{2}\chi + \frac{1}{2}\chi^3. \quad (2.8)$$

Considering the porous matrix as a system of capillaries with an averaged radius r_c and porosity ϕ_p one may assume that the velocity components for the Bingham fluid flow in this matrix are as follows (Walicka, 2011; Walicka and Walicki, 2011)

$$\bar{v}_x = \Psi(\Upsilon) \Phi_p \left(-\frac{\partial \bar{p}}{\partial x} \right), \quad \bar{v}_y = \Psi(\Upsilon) \Phi_p \left(-\frac{\partial \bar{p}}{\partial y} \right), \quad \Upsilon = \frac{2\tau_0}{\left(-r_c \frac{\partial \bar{p}}{\partial y} \right)} \quad (2.9)$$

where

$$\Phi_p = \frac{r_c^2 \phi_p}{2\mu}, \quad \Psi(\Upsilon) = \frac{1}{4} \left(1 - \frac{4}{3}\Upsilon + \frac{1}{3}\Upsilon^4 \right); \quad (2.10)$$

Φ_p is the permeability of the porous matrix, ϕ_p is the porosity.

Since the cross-velocity component \bar{v}_y must be continuous at the porous wall-fluid interface and must be equal to V , we have then, by virtue of Eqs (2.6) and (2.9)₂, the following form of the modified Reynolds equation

$$\frac{1}{R} \frac{\partial}{\partial x} \left[RH^3 \left(-\frac{\partial p}{\partial x} \right) \Phi(\chi) \right] = -12\mu \left[\dot{H} - \Psi(\Upsilon) \Phi_p \left(-\frac{\partial \bar{p}}{\partial y} \right) \Big|_{y=0} \right]. \quad (2.11)$$

Using the Morgan-Cameron approximation (Morgan and Cameron, 1957) one obtains

$$\Psi(\Upsilon) \Phi_p \left(-\frac{\partial \bar{p}}{\partial y} \right) \Big|_{y=0} = -\frac{H_p}{R} \frac{\partial}{\partial x} \left[R \Psi(\Upsilon) \Phi_p \left(-\frac{\partial \bar{p}}{\partial x} \right) \right]. \quad (2.12)$$

When formula (2.12) is inserted into Eq.(2.11) the modified Reynolds equation takes the form

$$\frac{1}{R} \frac{\partial}{\partial x} \left\{ R \left[H^3 \Phi(\chi) + 12\mu H_p \Phi_p \Psi(\Upsilon) \right] \left(-\frac{\partial p}{\partial x} \right) \right\} = -12\mu \dot{H} \quad (2.13)$$

where

$$\Upsilon = \chi \frac{H}{r_c} \quad \text{and} \quad \frac{\partial \bar{p}}{\partial x} = \frac{\partial p}{\partial x}. \tag{2.14}$$

If the film thickness is regarded as a random quantity, a height distribution function must be associated. Many real bearing surfaces show a roughness height distribution which is closely Gaussian, at least up to three standard deviations. From a practical point of view, the Gaussian distribution is rather inconvenient and therefore a polynomial form of its approximation is chosen. Following Christensen (1970; 1971; 1973) such a probability density function is

$$f(h_s) = \begin{cases} \frac{35}{32c^7} (c^2 - h_s^2)^3, & -c \leq h_s \leq +c \\ 0, & \text{elsewhere} \end{cases} \tag{2.15}$$

where c is the half total range of the random film thickness variable. The function terminates at $c = \pm 3\sigma$, where σ is the standard deviation.

Inserting expected values in Eq.(2.13) we get the general form of the stochastic Reynolds equation

$$\frac{1}{R} \frac{\partial}{\partial x} \left(E \left\{ R \left[H^3 \Phi(\chi) + 12\mu H_p \Phi_p \Psi(\Upsilon) \right] \left(-\frac{\partial p}{\partial x} \right) \right\} \right) = -12\mu E\dot{H} \tag{2.16}$$

where $E(\bullet)$ is the expectancy operator defined by

$$E(\bullet) = \int_{-c}^{+c} (\bullet) f(h_s) dh_s \tag{2.17}$$

The problem is now reduced to devising means of evaluating the left-hand side of Eq.(2.16) subject to the specific model of roughness.

The calculation of the mean film pressure distribution would require the evaluation of the expected value of various film thickness functions.

The general forms of the distribution function described by Eq.(2.17) are given in (Walicka, 2012).

3. Solutions to the modified Reynolds equation

Integration of Eq.(2.16) yields

$$E \left\{ R \left[H^3 \Phi(\chi) + 12\mu H_p \Phi_p \Psi(\Upsilon) \right] \left(-\frac{\partial p}{\partial x} \right) \right\} = -12\mu \int R E \dot{H} dx. \tag{3.1}$$

Assuming that the lubricant flow coincides with a flow with small core, then $\chi \ll 1, \Upsilon \ll 1$, and the functions $\Phi(\chi)$ and $\Psi(\Upsilon)$ become linear

$$\Phi(\chi) = 1 - \frac{3}{2}\chi, \quad \Psi(\Upsilon) = \frac{1}{4} \left(1 - \frac{4}{3}\Upsilon \right). \tag{3.2}$$

Substituting Eqs (3.2) into Eq.(3.1) and taking into account relations (2.7)₄ and (2.9)₃ we reach a formula

$$R \left[E \left(H^3 + \frac{3}{2} H_p r_c^2 \Phi_p \right) \left(-\frac{\partial E p}{\partial x} \right) - \tau_0 E \left(3H^2 + 4H_p r_c \Phi_p \right) \right] = -12\mu \int RE\dot{H}dx . \quad (3.3)$$

In the present study two types of roughness structure are of interest: the longitudinal (radial) one-dimensional roughness pattern, having the form of long narrow ridges and valleys running in the x direction, and the circumferential (transverse) one-dimensional roughness pattern, having the form of long narrow ridges and valleys running in the ϑ direction (Walicka and Walicki, 2002a; 2002b; Walicka, 2009). For the longitudinal one-dimensional roughness

$$H = h(x, t) + h_s(\vartheta, \xi) \quad (3.4)$$

the stochastic Reynolds equation is

$$R \left\{ \left[E \left(H^3 \right) + \frac{3}{2} H_p r_c^2 \Phi_p \right] \left(-\frac{\partial E p}{\partial x} \right) - \tau_0 \left[3E \left(H^2 \right) + 4H_p r_c \Phi_p \right] \right\} = -12\mu \int RE\dot{H}dx \quad (3.5)$$

but for the circumferential one-dimensional roughness

$$H = h(x, t) + h_s(x, \xi) \quad (3.6)$$

the stochastic Reynolds equation is

$$R \left\{ \left[\frac{1}{E \left(H^{-3} \right)} + \frac{3}{2} H_p r_c^2 \Phi_p \right] \left(-\frac{\partial E p}{\partial x} \right) - \tau_0 \left[\frac{3}{E \left(H^{-2} \right)} + 4H_p r_c \Phi_p \right] \right\} = -12\mu \int RE\dot{H}dx . \quad (3.7)$$

Note that both Eqs (3.5) and (3.7) may be presented in one common form as follows

$$R \left[\left(H_j^{(3)} + \frac{3}{2} H_p r_c^2 \Phi_p \right) \left(-\frac{\partial E p}{\partial x} \right) - \tau_0 \left(3H_j^{(2)} + 4H_p r_c \Phi_p \right) \right] = -12\mu \int RE\dot{H}dx \quad (3.8)$$

where

$$H_j^{(2)} = \begin{cases} E \left(H^2 \right) & \text{for } j = l, \\ \frac{1}{E \left(H^{-2} \right)} & \text{for } j = c, \end{cases} \quad H_j^{(3)} = \begin{cases} E \left(H^3 \right) & \text{for } j = l, \\ \frac{1}{E \left(H^{-3} \right)} & \text{for } j = c; \end{cases} \quad (3.9)$$

the case $j = l$ refers to the longitudinal one-dimensional roughness, but the case $j = c$ – to the circumferential one-dimensional roughness.

Introducing the notations

$$M_j^{(2)} = 3H_j^{(2)} + 4H_p r_c \Phi_p, \quad M_j^{(3)} = H_j^{(3)} + \frac{3}{2} H_p r_c^2 \Phi_p, \quad (3.10)$$

one may present the solution of Eq.(3.8) in the form

$$Ep = p_o + [F_o - F(x,t)] \tag{3.11}$$

where

$$I(x,t) = \int \frac{RE\dot{H}dx}{RM_j^{(3)}} dx, \quad J(x,t) = \int \frac{M_j^{(2)}}{M_j^{(3)}} dx, \tag{3.12}$$

$$F(x,t) = I2\mu I(x,t) + \tau_o J(x,t), \quad F_o = F(x_o, t);$$

The load-carrying capacity is defined by

$$N = 2\pi \int_0^{x_o} (Ep - p_o) R \cos \varphi dx; \tag{3.13}$$

the sense of angle φ arises from Fig.1.

The calculation of the mean film pressure distribution would require the evaluation of the expected value of various film thickness functions. For the distribution function given by Eq.(2.17) we have (Walicka, 2012)

$$E(H) = h, \quad E(H^2) = h^2 \left(1 + \frac{1}{9} Y^2 \right), \quad E(H^3) = h^3 \left(1 + \frac{1}{3} Y^2 \right),$$

$$E(H^{-2}) = \frac{1}{h^2} \left\{ 1 + \sum_{n=1}^{\infty} \frac{105Y^{2n}}{(2n+3)(2n+5)(2n+7)} \right\}, \quad Y = \frac{c}{h}, \tag{3.14}$$

$$E(H^{-3}) = \frac{1}{h^3} \left\{ 1 + \sum_{n=1}^{\infty} \frac{105(n+1)Y^{2n}}{(2n+3)(2n+5)(2n+7)} \right\},$$

4. Axial squeeze film bearing

An axial squeeze film bearing is modelled by two parallel disks (Fig.2). Introducing the following parameters

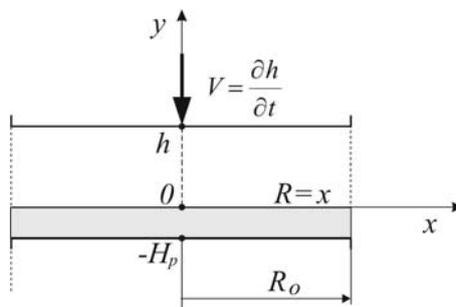


Fig.2. Axial squeeze film bearing.

$$\begin{aligned} \tilde{x} &= \frac{x}{x_o}, & R &= x, & \tilde{R} &= \frac{R}{R_o}, & \tilde{h} &= \frac{h}{h_o} = e(t), & e(t) &= 1 - \varepsilon(t), \\ K_p &= \frac{r_c}{h_o}, & \tilde{H}_p &= \frac{H_p \Phi_p}{h_o}, & \tilde{p} &= \frac{(Ep - p_o) h_o^3}{\mu V_o x_o^2}, & V_o &= h_o \dot{\varepsilon}, \\ \tilde{N} &= \frac{N h_o^3}{\mu V_o x_o^4}, & SV &= \frac{\tau_o h_o^2}{\mu V_o x_o}, \end{aligned} \quad (4.1)$$

where SV is the Saint-Venant plasticity number (plasticity index), one may present formulae (3.11) and (3.13) in simple non-dimensional forms

$$\tilde{p}(\tilde{x}, t) = D(1 - \tilde{x}^2) + E(1 - \tilde{x}) \quad (4.2)$$

and

$$\tilde{N} = \frac{\pi}{2} \left(D + \frac{2}{3} E \right). \quad (4.3)$$

Here

$$D = \frac{3}{\tilde{H}_j^{(3)} + \frac{3}{2} \tilde{H}_p K_p^2}, \quad E = \frac{3\tilde{H}_j^{(2)} + 4\tilde{H}_p K_p}{\tilde{H}_j^{(3)} + \frac{3}{2} \tilde{H}_p K_p^2} SV, \quad (4.4)$$

and

$$\tilde{H}_j^{(2)} = \begin{cases} e^2 \left[1 + \frac{1}{9} \left(\frac{c^*}{e} \right)^2 \right] & \text{for } j=l, \\ \left(\frac{1}{e^2} \left[1 + \frac{1}{3} \left(\frac{c^*}{e} \right)^2 \right] \right)^{-1} & \text{for } j=c, \end{cases} \quad (4.5)$$

$$\tilde{H}_j^{(3)} = \begin{cases} e^3 \left[1 + \frac{1}{3} \left(\frac{c^*}{e} \right)^2 \right] & \text{for } j=l, \\ \left(\frac{1}{e^3} \left[1 + \frac{2}{3} \left(\frac{c^*}{e} \right)^2 \right] \right)^{-1} & \text{for } j=c, \end{cases} \quad c^* = \frac{c}{h_o}.$$

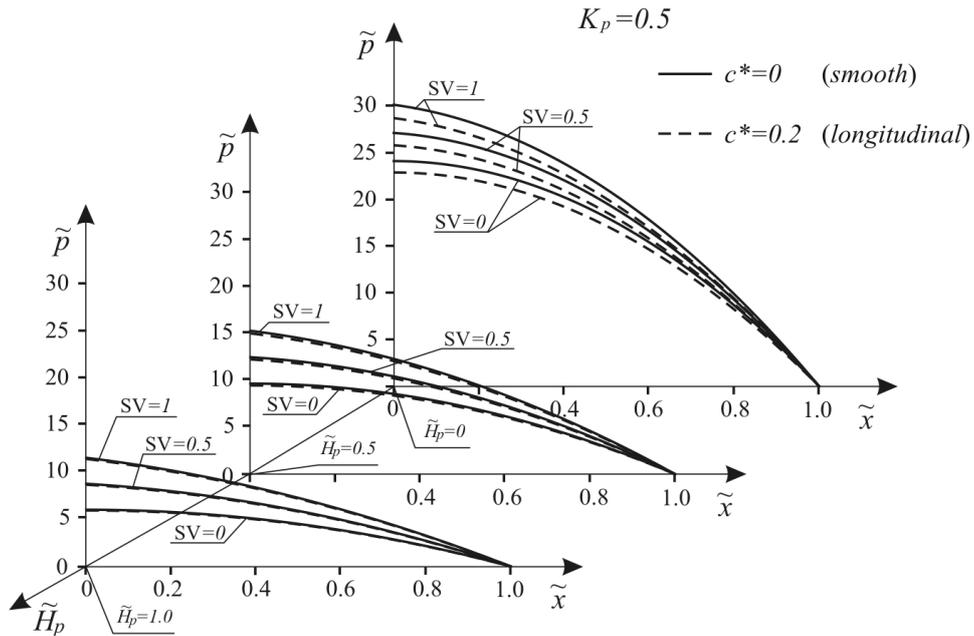


Fig.3. Dimensionless pressure distribution of the thrust bearing with rough surfaces for longitudinal roughness for $K_p = 0.5$; $\varepsilon = 0.5$ and for different values of $SV = 0; 0.5; 1.0$.

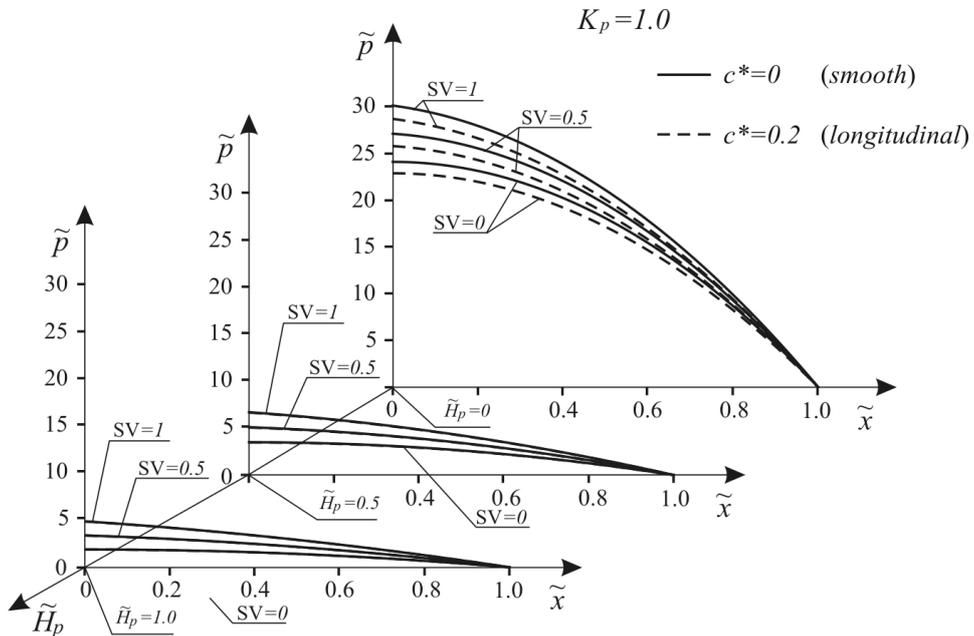


Fig.4. Dimensionless pressure distribution of the thrust bearing with rough surfaces for longitudinal roughness for $K_p = 1.0$; $\varepsilon = 0.5$ and for different values of $SV = 0; 0.5; 1.0$.

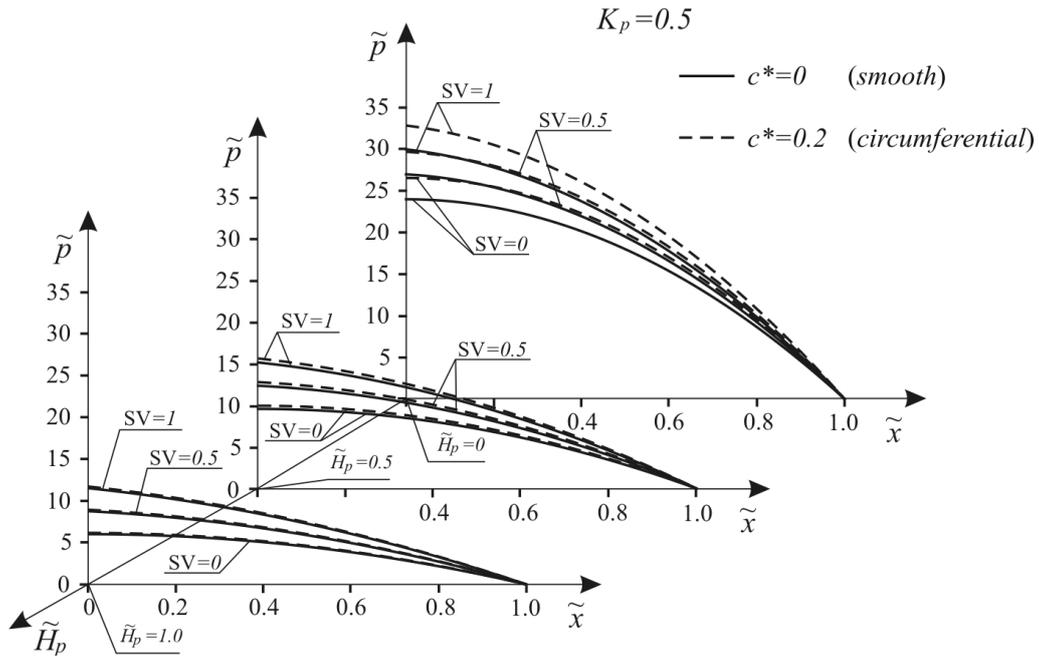


Fig.5. Dimensionless pressure distribution of the thrust bearing with rough surfaces for circumferential roughness for $K_p = 0.5$; $\varepsilon = 0.5$ and for different values of $SV = 0; 0.5; 1.0$.

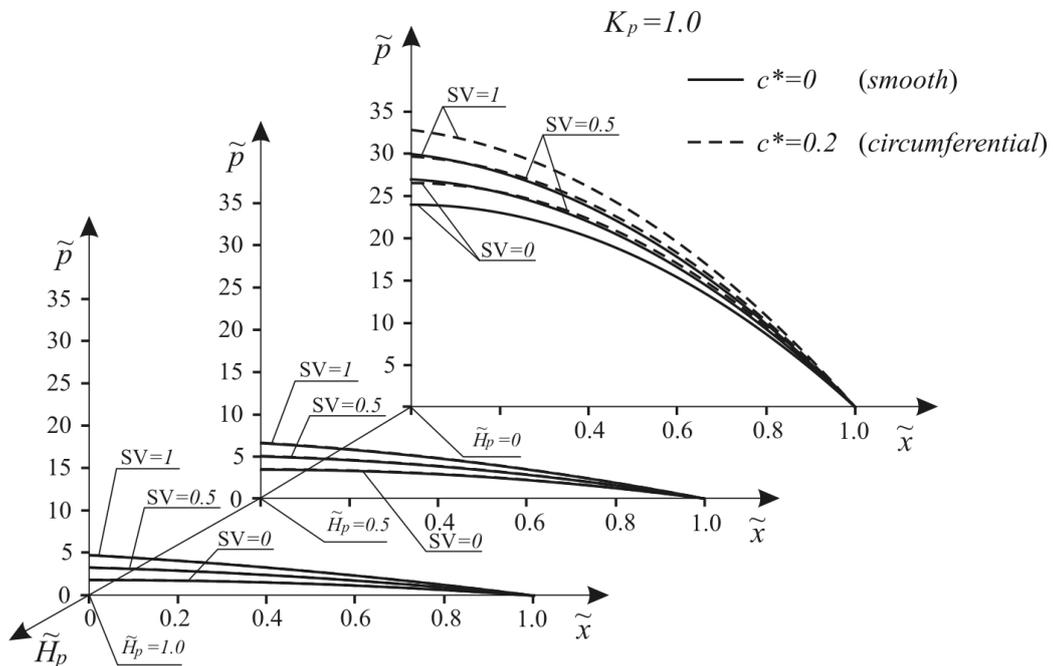


Fig.6. Dimensionless pressure distribution of the thrust bearing with rough surfaces for circumferential roughness for $K_p = 1.0$; $\varepsilon = 0.5$ and for different values of $SV = 0; 0.5; 1.0$.

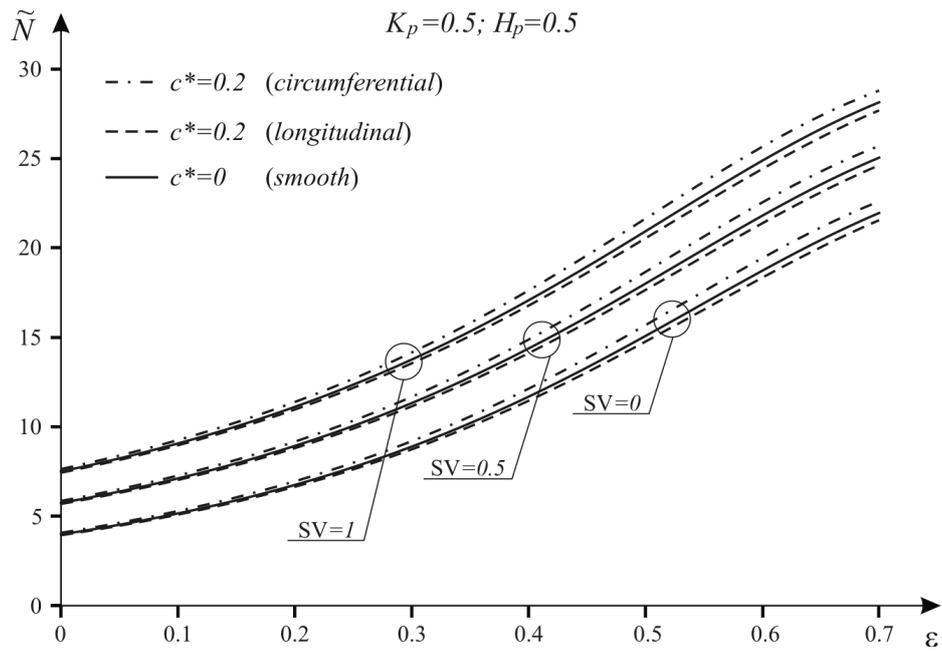


Fig.7. Load carrying capacity of the thrust bearing with rough surfaces for circumferential roughness for $K_p = 0.5$ and for different values of $SV = 0; 0.5; 1.0$.

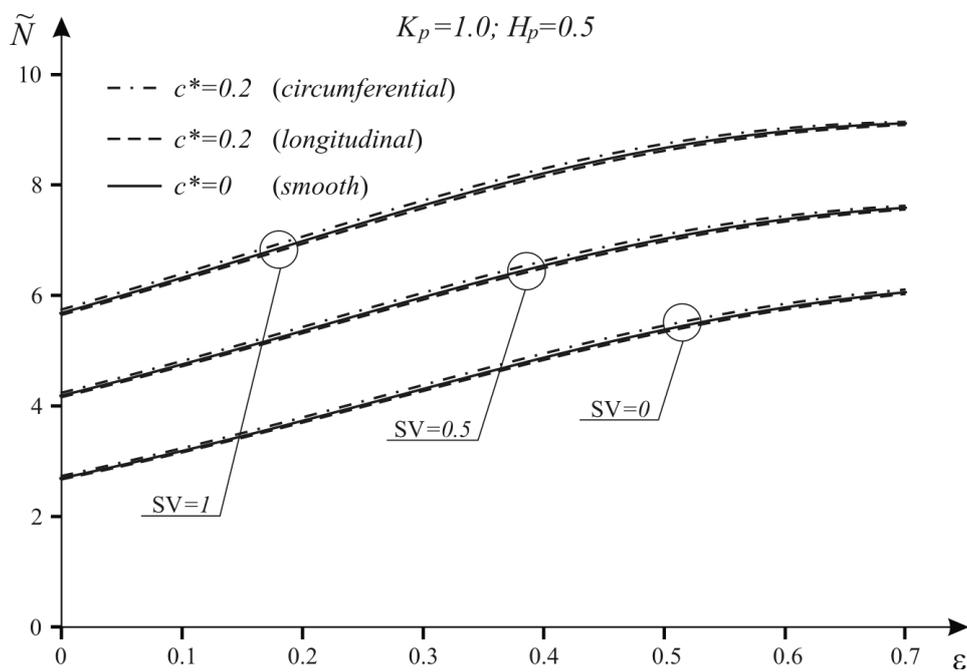


Fig.8. Load carrying capacity of the thrust bearing with rough surfaces for circumferential roughness for $K_p = 1.0$ and for different values of $SV = 0; 0.5; 1.0$.

5. Conclusions

The modified Reynolds equation for a Bingham type of viscoplastic lubricants flowing in a clearance of a thrust curvilinear bearing with rough surfaces is obtained. As a result the general formulae for pressure distributions and load-carrying capacity are derived. It follows from theoretical considerations, numerical calculations and their graphic presentations that both the magnitudes are dependent on the rheological parameter SV being the de Saint-Venant plasticity number and on the geometric parameters characterizing the bearing clearance and porous layer. It may be concluded that generally the pressure and load-carrying capacity increase with the increase of the values of SV .

Both these values decrease with the increase of porosity K_p and thickness \tilde{H}_p of the porous layer. The bearing surface roughness, expressed by c^* , results in some small increase of the values of bearing mechanical parameters for circumferential roughness and in a small decrease for longitudinal roughness.

Nomenclature

- A_I – the first Rivlin-Ericksen kinematic tensor
- c – maximum asperity deviation
- c^* – nondimensional roughness parameter
- $E(\bullet)$ – expectancy operator
- $e(t)$ – bearing squeezing
- $f(h_s)$ – probability density distribution function
- H – film thickness
- H_p – porous pad thickness
- $h(x,t)$ – nominal film thickness
- $h_s(x, \vartheta, \xi)$ – random deviation of film thickness
- K_p – porosity
- k, k_i – pseudo-plasticity coefficients
- N – load-carrying capacity
- p – pressure
- $R, R(x)$ – local radius of the lower bearing surface
- r – radius
- SV – de Saint-Venant plasticity number (plasticity index)
- v_x, v_y – velocity components
- x, y – orthogonal coordinate
- $\varepsilon(t)$ – squeezing ratio
- ϑ – angular coordinate
- μ – coefficient of viscosity
- ξ – random variable
- ρ – fluid density

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